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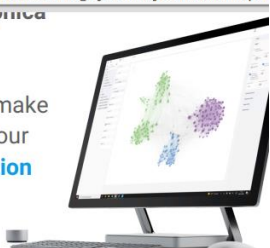
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"Comparison of Immobilized and Free Amyloglucosidase Process in Glucose Syrups Production from White Sorghum Starch."

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Author	Response to Reviewers

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cbdv.202300071

"Comparison of Immobilized and Free Amyloglucosidase Process in Glucose Syrups Production from White Sorghum Starch."

Original Submission

Astrilia Damayanti (Reviewer 1)

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Note 1. 1. CaCl ₂ is not an immobilized matrix but a cross-linking agent. So this research is not appropriate to vary 2. 2. The recovery of CaCl ₂ and Na-alginate is not explained 3. 3. From fig. 4 that the field of free >>> is immobilized so it doesn't match the abstract in lines 39-40 4. 4. Research on immobilization of enzymes with calcium alginate reported by Dey et al. [27]. So this research does not have a state of the art. G. Dey, S. Bhupinder, R. Banerjee, 'Immobilization of alpha-amylase produced by <i>Bacillus circulans</i> GRS 313', <i>Braz. Arch. Biol. Technol.</i> 2003, 46, 167-176. https://doi.org/10.1590/s1516-89132003000200005	
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Comparison of Immobilized and Free Amyloglucosidase Process in Glucose Syrups Production from White Sorghum Starch.

--Manuscript Draft--

Manuscript Number:	cbdv.202300071
Article Type:	Research Article
Order of Authors:	Houria Taibi Nadia Boudries, Ph.D Moufida Abdelhai, PhD student Hakim Lounici
Full Title:	Comparison of Immobilized and Free Amyloglucosidase Process in Glucose Syrups Production from White Sorghum Starch.
Keywords:	Calcium alginate beads; Glucose syrups; Immobilization; Saccharification; White sorghum starch
Manuscript Classifications:	Catalysis; Materials Science: General; Sustainable Chemistry
Abstract:	<p>Optimum conditions for production glucose syrups from white sorghum were studied through sequential liquefaction and saccharification processes. In liquefaction process, a maximum dextrose equivalent (DE) of 10.98% was achieved using 30% (w/v) of starch as using Termamyl α-amylase from <i>Bacillus licheniformis</i> and saccharification was done by free or immobilized amyloglucosidase from <i>Rhizopus</i> mold at 1% (w/v). DE values of 88.32% and 79.95% were obtained from 30% (w/v) of starch respectively with free and immobilized enzyme. The immobilized Amyloglucosidase in calcium alginate beads showed reusable capacity for up to 6 cycles with 46% of the original activity retained. The kinetic behaviour of immobilized and free enzyme gives K_m value of 22.13 and 16.55 mg mL⁻¹ and V_{max} of 0.69 and 1.61 mg mL⁻¹ min⁻¹, respectively. The hydrolysis yield using immobilized amyloglucosidase were lower than that of the free one. However, it relevant to reuse enzyme without losing activity in order to increase overall starch transformation into required products in industrial manufacturing. Hydrolysis of sorghum starch using immobilized amyloglucosidase can be a promising alternative towards the development of the glucose syrups production process and its utilization for several industries.</p>

1 **Comparison of Immobilized and Free Amyloglucosidase Process in Glucose**
2 **Syrups Production from White Sorghum Starch.**

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26 **Abstract**

27 Optimum conditions for production glucose syrups from white sorghum were studied through
28 sequential liquefaction and saccharification processes. In liquefaction process, a maximum
29 dextrose equivalent (DE) of 10.98% was achieved using 30% (w/v) of starch as using
30 Termamyl α -amylase from *Bacillus licheniformis* and saccharification was done by free or
31 immobilized amyloglucosidase from *Rhizopus mold* at 1% (w/v). DE values of 88.32% and
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39 products in industrial manufacturing. Hydrolysis of sorghum starch using immobilized
40 amyloglucosidase can be a promising alternative towards the development of the glucose
41 syrups production process and its utilization for several industries.

42 **Keywords:** Calcium alginate beads, Glucose syrups, Immobilization, Saccharification, White
43 sorghum starch.

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54 **Introduction**

55 Glucose syrup is a carbohydrate frequently utilized in food processing and other
56 industries. It is considered as a major ingredient in confectionery products for their anti-
57 crystallizing properties and in brewing for their sweetening capacity. ^[1] Also, it is useful in
58 pharmaceutical and industrial fermentations. ^[2] Corn starch is the widespread raw material
59 used to produce glucose syrup, which accounts for approximately 80% of global starch
60 production. ^[3] However, due the increase demand for glucose syrup, other unconventional
61 sources of starch such as cassava, sorghum has also been examined as a potential source of
62 glucose syrup. ^[4, 5]

63 Over the last two decades, sorghum (*Sorghum bicolor* (L.) Moench) starch has
64 received widespread attention due to its specific properties and the ability of sorghum to adapt
65 to drought, disease and poor soil quality. Especially to its relevance as a food and industrial
66 crop, particularly their prominent potential health benefits due to high starch content and its
67 nutritional contribution at the agro-industrial level and processing applications. ^[6, 7] In hyper-
68 arid regions of Algeria, Many landraces and domesticated sorghum were cultivated ^[8] and
69 still undervalued although it may be an alternative source to the conventional crops. Previous
70 studies ^[9] have revealed that white sorghum starch is an interesting source of glucose syrups
71 production due to the starch contents in kernel around 60-70 % and interesting thermal and
72 rheological properties influenced by their environmental and genotypic effects. ^[10, 11]

73 The industrial starch processing of syrup glucose may be realised by enzyme and acid
74 hydrolysis or a combination of the two. Due to the disadvantages of using acid hydrolysis, the
75 enzymatic hydrolysis is the most widely used methods because of its better control of the
76 process and the resulting products. Using α -amylase for liquefaction starch to dextrins,
77 subsequently, the sugar chains are further broken down by the amyloglucosidase during the
78 saccharification process to produce simple glucose syrup with a high dextrose equivalent
79 (DE). ^[12, 13]

80 Enzymes are of great interest in the field of biocatalysis in food. However, their cost
81 and their limited stability over time are factors limiting their use. In order to overcome these
82 drawbacks, a strategy was proposed: the immobilization of enzymes, which allows improving
83 stability of the enzyme and convenience of their reuse in bioreactor systems. ^[14] The stability
84 of the confined enzyme is determined by the intrinsic nature of the enzyme, the conditions of
85 immobilization, the nature of the support material used and the conditions of reactions. ^[15]

86 Immobilization of amyloglucosidase has been used in the saccharification process for
87 the continuous conversion of the starch in order to produce glucose syrups. Many interesting
88 studies were focused on techniques, such as covalent adsorption, binding and cross-linking for
89 entrapment of amyloglucosidase into insoluble supports ^[16] as non-porous polystyrene/poly
90 (sodium styrene sulfonate) (PS/PNaSS), ^[17] Poly [(glycidyl methacrylate) Co(ethylene
91 dimethacrylate)] ^[16, 18], polyglutaraldehyde-activated gelatin, chitosan and amberlite beads,
92 ^[16, 19] magnetic nano-particles ^[20, 21] and alginate fibers, ^[22] but the most common supports for
93 enzyme immobilization are calcium alginate beads. They are appreciated for their good
94 biocompatibility, ease of preparation, low cost and easy availability. ^[23] For these benefits, the
95 purpose of this research was to evaluate the performance of calcium alginate beads as a
96 support material for *Rhizopus mold* amyloglucosidase entrapment and their subsequent
97 utilisation in the hydrolysis of white sorghum starch. It involves the determination of
98 optimum conditions of immobilization and glucose syrups production. Furthermore,
99 liquefaction of white sorghum starch was examined and optimized using heat stable *Bacillus*
100 *licheniformis* α -amylase. ^[9]

101 **Results and Discussion**

102 The achieved essays aimed to highlight performance efficiency of amyloglucosidase
103 immobilization in alginate beads on the saccharification process to attain the best conditions
104 for glucose syrups production from an interesting isolated white sorghum starch that grows in
105 hyper-arid regions of Algeria.

106 *Optimization of calcium alginate beads properties*

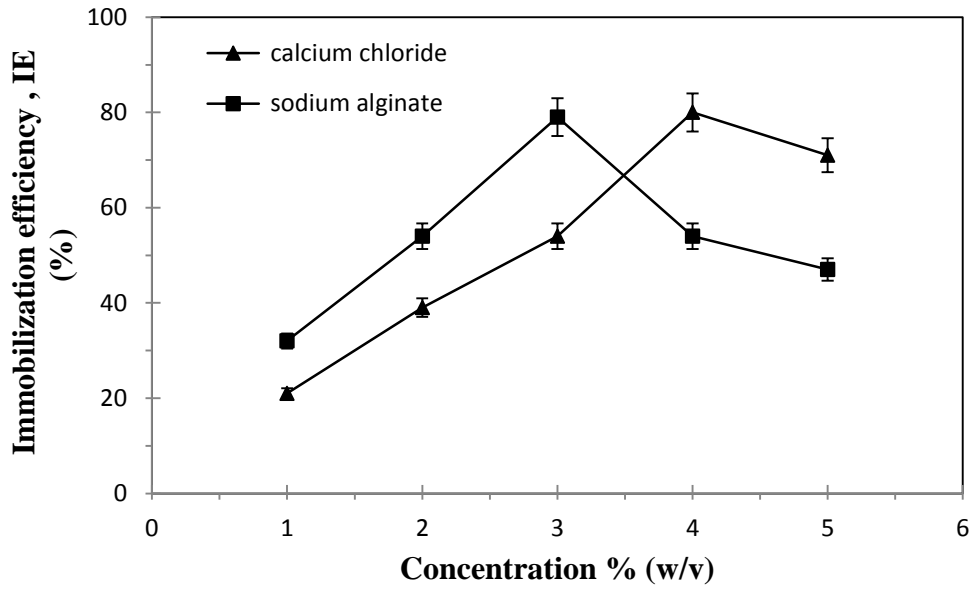
107 The calcium alginate beads are frequently used carriers in the encapsulation of
108 biocatalyst due to their significant advantages such broad availability, cost effectiveness, good
109 biocompatibility without toxicity and light gelation conditions. ^[24] In addition, this
110 polysaccharide is adopted in several applications as the supporting material for release
111 encapsulated cells and enzymes in the food and pharmaceutical industries. ^[25] The calcium
112 chloride and sodium alginate are the most important components affecting the performance of
113 amyloglucosidase immobilization in alginate. For this, the effect of their concentration was
114 examined with the range of 1 to 5% (w/v) to attain an efficient immobilization of
115 amyloglucosidase on alginate beads with desired mechanical strength.

116 The results revealed that amyloglucosidase was effectively confined using that interval
117 of sodium alginate concentrations. However, the optimal concentration was 3% (w/v) as
118 clearly seen in Figure1. It gave a maximum IE of 79 %, whereas, the lower IE of 32% was
119 obtained with 1% (w/v). It might be due to less tightly cross-linked alginate gel and larger
120 pore size of the beads ^[26] which allowed a greater enzyme leakage from beads. ^[27, 28] In the
121 case of increasing concentrations of sodium alginate more than 3% (w/v), the IE decreased
122 gradually due to the increased viscosity in the solution to form the beads, leading to smaller
123 cavities size in the beads and diffusion limitation of the substrate to the active site of the
124 enzyme. ^[27, 29]

125 Additionally, the effect of calcium chloride concentration (1-5 %, w/v) at 3% (w/v)
126 constant sodium alginate concentration on immobilization efficiency was tested (*Figure 1*).

127 The results, as shown, in *Figure 1* revealed an increase of immobilization efficiency
128 with increasing calcium chloride concentration up to 4% (w/v). It has been due probably to an
129 increase in the cross-linking density of beads and the concomitant decrease in enzyme as
130 explained by many authors as Konsoula et al. ^[23] and Priyanka et al. ^[29] Above 4% (w/v) of
131 calcium chloride, enzyme activity decreases owing to a change in pH and its effect on the
132 activity of confined enzyme. ^[30]

133 In order to investigate the conditions for the obtaining stable beads with an appreciable
134 concentration of confined enzyme, the sodium alginate and calcium chloride concentrations
135 were fixed at 3 and 4% (w/v), respectively. The beads were incubated for 30 to 120 min to
136 determine the appropriate hardening time for improving the immobilization yield. The highest
137 IE was obtained at the optimum hardening time of 90 minutes (*Figure 2*). Above 120 min, the
138 activity of amyloglucosidase was decreased caused by leakage of amyloglucosidase from the
139 beads as reported by Dey et al. ^[27]

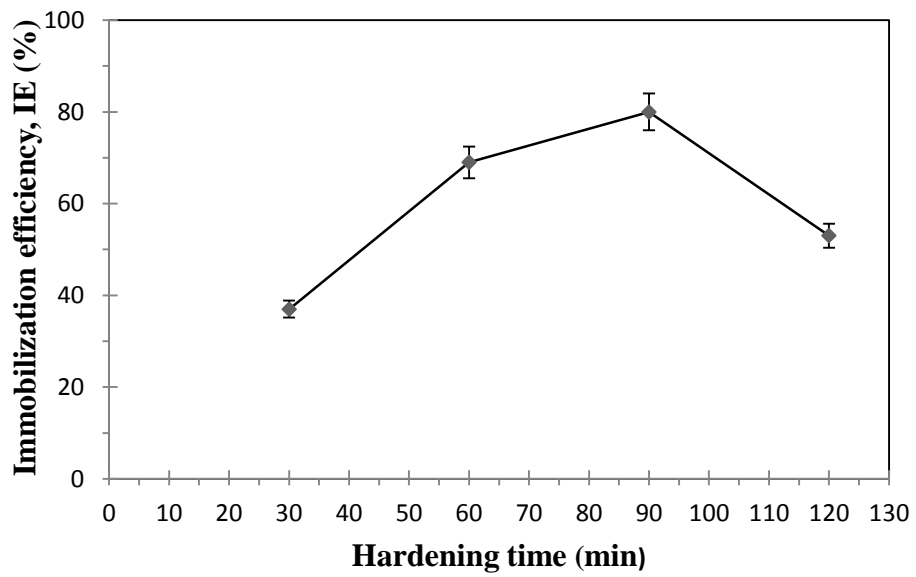


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Figure 1. Effect of concentration of calcium chloride and sodium alginate on immobilization efficiency, IE.



143

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Figure 2. Effect of hardening time on immobilization yield.

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146

At the best immobilization conditions, regular and spherical shape of the calcium alginate beads was obtained, as illustrated in *Figure 3*.



147

148 **Figure 3.** The Spherical shape of the calcium alginate beads (original, 2021).

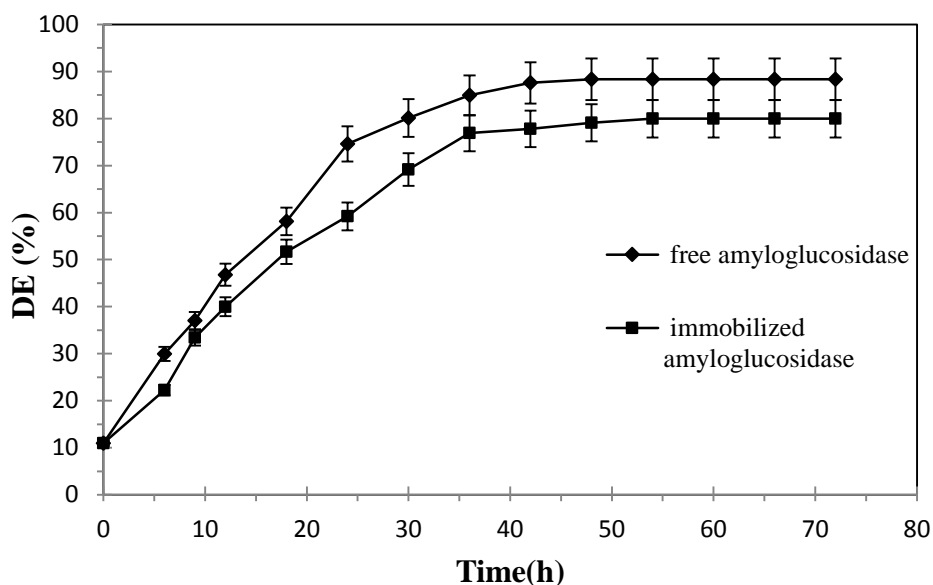
149

Saccharification of liquefied white sorghum Starch

150 Monitoring of the saccharification process for 72 hours has been carried out to study
151 the evolution of DE using, respectively, free and immobilized amyloglucosidase and to
152 compare their efficiencies under the same conditions. *Figure 4* shows the results of
153 continuously saccharification of liquefied white sorghum starch for free and immobilized
154 amyloglucosidase.

155 A lower yield ($79.95 \pm 0.08\%$) of DE was produced by the immobilized enzyme
156 compared to free enzyme ($88.32 \pm 0.25\%$). Both amyloglucosidase systems achieved their
157 maximum DE yields within 48 to 54 hours. The saccharification (first run) with free
158 amyloglucosidase was found more efficient with an increase of 8% approximately in the DE
159 than that of immobilized amyloglucosidase. The contact between the free amyloglucosidase
160 and its substrate is more efficient because both have a high degree of freedom, increasing the
161 probability for one coming into close contact with the other. ^[31] However, as a result of
162 immobilization, the yield of obtained DE decreased. It may be caused by the enzymes'
163 restricted ability to reach substrate molecules at their active sites, their interaction with
164 functional groups on the surface of beads, or their extensive surface contact with supports.

165 However, although the yield with immobilized amyloglucosidase was lower, the
166 ability to reuse amyloglucosidase is of enormous relevance from operational and economic
167 aspects, particularly due to the high cost of the enzymes which present the major duress in
168 their industrial application.



169

170 **Figure 4.** Kinetic of white sorghum starch saccharification at 30% (w/v)
 171 using free and immobilized amyloglucosidase.

172 *Effect of amyloglucosidase immobilization on Kinetic hydrolysis*

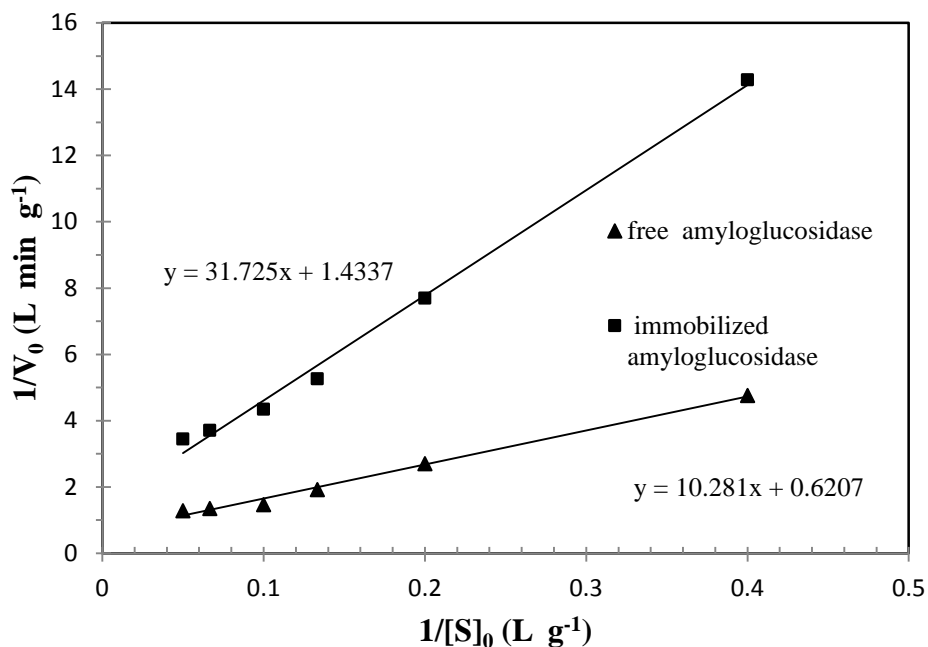
173 The kinetic constants V_{max} and K_m of both free and immobilized amyloglucosidase
 174 were determined using Lineweaver-Burk plots (*Figure 5*). A K_m of 16.55 and 22.13 mg mL⁻¹
 175 and a V_{max} of 1.61 and 0.69 mg mL⁻¹min⁻¹ were obtained, respectively, for free and
 176 immobilized enzyme as mentioned in *Table 1*. The results revealed that after immobilization
 177 of amyloglucosidase in calcium alginate beads, K_m was amplified by 5.58 mg mL⁻¹, while,
 178 V_{max} was reduced at 0.92 mg mL⁻¹ min⁻¹. It might be due to the hindrance of the substrate to
 179 penetrate in beads for enzyme-substrate reaction. [32]

180 **Table 1.** Kinetic parameters of white sorghum starch hydrolysis using free and immobilized
 181 amyloglucosidase.

Enzyme	V_{max} (mg mL ⁻¹ min ⁻¹)	K_m (mg mL ⁻¹)
Free amyloglucosidase	1.61	16.55
Immobilized amyloglucosidase	0.69	22.13

186 Similar results have been reported about the increase in K_m and decrease in V_{max} of
 187 alpha-amylase, urease [33] and amyloglucosidase entrapped in the agar- agar matrix. [34] Pervez

188 et al. [35] have also obtained significantly larger K_m and lower V_{max} for immobilized
 189 amyloglucosidase compared to the free form. However, no change was found for the affinity
 190 of amylase towards soluble starch after it was confined in calcium agar tablets, whereas a
 191 higher augmentation was observed. [36]



192

193 **Figure 5.** Lineweaver–Burk plots of white sorghum starch hydrolysis
 194 using free and immobilized amyloglucosidase.

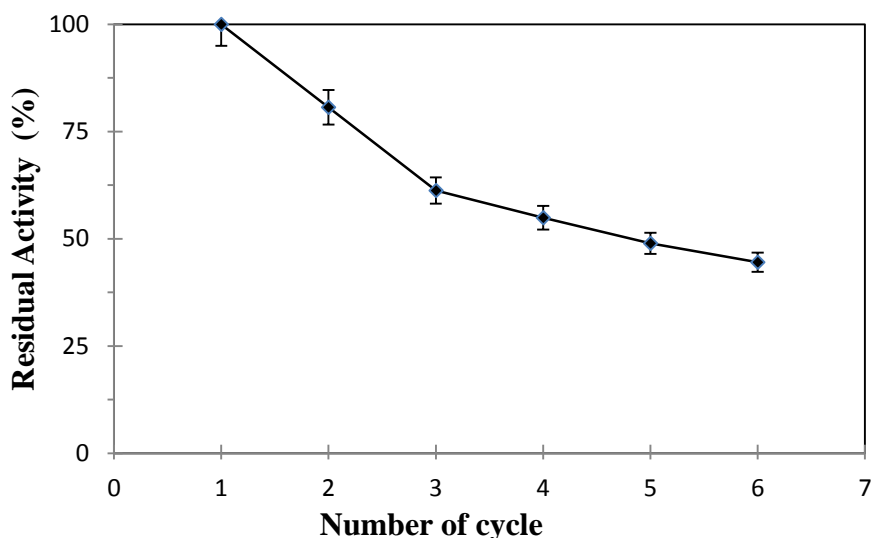
195 *Operational stability of Immobilized amyloglucosidase*

196 One of the most significant advantages of the reusability of enzyme is its positive
 197 effect on the economic side by lower costs of glucose syrups production due to reducing
 198 consumption of enzyme. Therefore, the main goal of the current work was to patten an
 199 immobilization method that can retrieve amyloglucosidase from the reaction mixture in order
 200 to ensure its continued reuse for glucose syrup production.

201 The operational stability of enzymes is one of the most significant factors influencing
 202 performance of an immobilized enzyme system for utilisation in industrial bioprocess. For
 203 this reason, the reusability of amyloglucosidase entrapped was examined at 60 °C and the
 204 final DE concentration was determined over six cycles.

205 The results related to the reuse of confined enzyme were represented at the *Figure 6*.
 206 They showed that immobilized amyloglucosidase maintained its activity up to 81 and 46%

207 after the 2 and 6th recycles, respectively. [37] had reported that the glucoamylase from
208 *Aspergillus niger* (50 U mg⁻¹) retained 88 % of its original activity after 20th cycles. Gupta et
209 al.[16] obtained 43 successive reuse of immobilized amyloglucosidase obtained from solid
210 state fermentation of *Aspergillus niger* with 35% residual activity and Wang et al. [38] reported
211 that calcium-alginate entrapped enzyme can be reused up to 10 cycles with the remaining
212 activity of 56 %.



213

214 **Figure 6.** Reusability of immobilized amyloglucosidase.

215 The decrease in the amyloglucosidase activity could be due to repeated washing of the
216 beads after each cycle and/or in increasing the size of pores after repeated uses, leading to
217 increased leakage of the enzyme and activity reduction. [39, 40] The reduction in the activity
218 observed after multiple cycles at the final batches is, probably also, a consequence to different
219 factors as inherent wastes by the material transfer, but mainly due to the denaturation of the
220 biocatalyst. [41]

221 **Conclusions**

222 The focus of this investigation revolves around the determination of optimum
223 conditions for glucose syrups production from undervalued white sorghum starch with
224 appreciable yield using enzymes in both liquefaction and saccharification processes. In
225 addition, the optimization of the amyloglucosidase immobilization in calcium alginate was
226 studied. The performances of confined and free amyloglucosidase were compared and it
227 seems to be different as expected. An optimal initial concentration of 30% (w/v) of white
228 sorghum starch and 0.1% (w/v) of free Termamyl α -amylase were used for liquefaction and

229 final DE of 10.98% was attained at the end of the saccharification step, DE increases until it
230 reaches 79.95% and 88.32% using, respectively, immobilized and free amyloglucosidase and
231 the immobilization efficiency was maintained until the sixth use.

232 However, the immobilized amyloglucosidase system may be an economically feasible
233 glucose syrups production process for its easy separation from the substrate, allowing the
234 reuse of the amyloglucosidase which could reduce the costs of the process, highlighting its
235 potential for possible application in the production of glucose syrups. In addition, there is an
236 opportunity to improve the glucose syrups yield from the starch isolated from Algeria white
237 sorghum landrace cultivated in hyper-arid regions of with fewer costs by improvement of
238 techniques for immobilization amyloglucosidase to enable the long-term re-usability of the
239 enzyme and also the separation of catalyst more easily from the hydrolysates.

240 **Experimental Section**

241 Selected white sorghum landrace was cultivated in In Salah, a region of the Sahara of
242 Algeria where high temperatures and very low rainfall were registered.

243 For hydrolysis process, *Bacillus licheniformis* α -amylase (Termamyl®300L Type DX,
244 300 KNU/g) and *Rhizopus mold* amyloglucosidase (23000 U/g) were used, respectively, for
245 enzymatic liquefaction and saccharification. All chemical reagents were of analytical quality.

246 *Isolation and purification of white sorghum starch*

247 The alkaline method ^[42] was used to isolate and purify starch from grains of Algerian
248 white sorghum. The different steps involve swelling in 0.20% (w/v) of NaOH, wet-milling,
249 sieving (1000, 355, 50 μ m), centrifugation (5000 rpm during 20 min) and lastly dried at 40°C.
250 ^[10]

251 *Amyloglucosidase activity determination*

252 The activity of amyloglucosidase was measured by determination of starch hydrolysis
253 rate. The liberated reducing sugar was determined by DNS acid method. ^[43] The enzymatic
254 hydrolysis reactions were carried out using the Sigma method, ^[44] using white sorghum starch
255 (1%, w/v) as a substrate in sodium acetate buffer (0.05 M, pH 4.5) at 40°C and glucose as the
256 standard. This method consists of hydrolysing starch into reducing sugars. One unit of
257 glucoamylase activity is defined as the amount of enzyme that produces 1.0 μ mol of glucose
258 from dissolubility starch per minute under the assay conditions. ^[37]

259 *Immobilization of Amyloglucosidase onto the calcium alginate beads*

260 The entrapment of amyloglucosidase in calcium alginate beads, was realized
261 according to Roy et al. [45] by mixing aqueous sodium alginate (3%, w/v) and (1%, w/v) of
262 *Rhizopus mold* amyloglucosidase in acetate buffer (0.05 M, pH 4.5). A volume of 50 mL of
263 the mixture were drip-fed through a syringe into a calcium chloride solution (4%, w/v) under
264 strict magnetic agitation. The produced beads were recovered by filtration, thoroughly rinsed
265 with distilled water to remove excess calcium chloride and unbound enzyme molecules and
266 then kept in sodium acetate buffer in a refrigerator until use.

267 *Optimization of the calcium alginate beads properties*

268 Bead properties were studied using beads of different permeability and rigidity in
269 order to find the best conditions to have the best properties. The effect of sodium alginate
270 concentration on the bead permeability was investigated using various concentrations of
271 sodium alginate (1- 5%, w/v) and the effect of calcium chloride concentration on the rigidity
272 of the beads was examined at different concentrations of calcium chloride solution (1- 5%,
273 w/v). The effect of hardening time on the catalytic activity of immobilized amyloglucosidase
274 was also determined using the optimal concentrations of alginate de sodium and calcium
275 chloride solutions for times ranging between 30.0 and 120.0 min.

276 *Determination of immobilization efficiency of the amyloglucosidase*

277 The immobilization efficiency (IE) was calculated as the yield for confined
278 amyloglucosidase in the calcium alginate beads according to the following equation (1):

279
$$IE (\%) = \frac{\text{Activity of immobilized Amyloglucosidase}}{\text{Activity of free Amyloglucosidase}} \times 100 \quad (1)$$

280 *Kinetic Parameters determination*

281 The maximum initial velocity, V_{\max} , and the concentration of substrate which permits
282 the enzyme to achieve half maximum initial velocity, K_m of immobilized and free
283 amyloglucosidase were determined from Lineweaver-Burk Plot using initial rates of
284 hydrolysis catalyzed by free or immobilized enzyme using various concentrations of starch
285 substrate (2.5 to 20.0 mg/mL).

286 *Saccharification of Liquefied white sorghum Starch*

287 The liquefaction of white sorghum starch was optimized in previous study using from
288 heat stable *Bacillus licheniformis* α -amylase.^[9] The liquefied starch was adjusted to pH 4.5
289 with 1 M HCl, then, 30 % (w/v) of liquefied sorghum starch was mixed with 1% (w/v) of
290 free amyloglucosidase or equivalent units of alginate immobilized amyloglucosidase beads
291 (about 2g of prepared beads under optimal conditions). The reaction mixture was incubated at
292 60°C for 72 h, to produce glucose syrup with high DE. During incubation, the samples were
293 taken every 6 h until 72 h and the dextrose equivalent was determined. At the end of each run,
294 sodium carbonate Na₂CO₃ solution was added to syrup glucose to remove the free acid and
295 then activated carbon was used for purification of product produced by adsorption and
296 vacuum filtration. Total refined glucose syrup was concentrated in Buchi Rotavapor model R-
297 114.

298 *Operational stability of Immobilized amyloglucosidase determination*

299 Beads were removed from the end of saccharification process and mixture was by
300 sifting, washed thoroughly with distilled water. The new medium using fresh substrate was
301 added and the saccharification was continued. The same process was repeated until the 8th
302 use. Percent remaining activity was determined by taking the enzyme activity of the first
303 cycle as 100%.

304 *Dextrose equivalent value estimation*

305 Dextrose equivalent, DE, was estimated as the concentration of reducing sugars
306 according to DNS acid method, as reported by Miller.^[46] A calibration curve was previously
307 established using glucose samples with known concentrations and using UV–Visible
308 spectrophotometer (shimadzu UV-Vis 1605) at 540 nm. DE values were given using the
309 following formula (2):

$$310 \quad DE = 100 \cdot \frac{\text{total mass of released glucose}}{\text{initial mass of starch}} \cdot (162/180) \quad (2)$$

311 *Statistical analysis*

312 All experiments were conducted in triplicate of each sample and results are notified as
313 mean \pm SD of the three values.

314

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322 Houria Taibi: Conceptualization, Methodology, Investigation, Writing - original draft.
323 Nadia Boudries: Conceptualization, Investigation, Writing - review & editing, Supervision.
324 Moufida Abdelhai: Writing - original draft. Hakim Lounici: review & editing, Supervision.

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